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         JUL 02
                 CHEMCATS accession numbers revised
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         JUL 02
                 CA/CAplus enhanced with utility model patents from China
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         JUL 16
                 CAplus enhanced with French and German abstracts
NEWS 18
         JUL 18
                 CA/CAplus patent coverage enhanced
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         JUL 26
                 USPATFULL/USPAT2 enhanced with IPC reclassification
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         AUG 06
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                 patents
         AUG 20
NEWS 25
                 CA/CAplus enhanced with CAS indexing in pre-1907 records
NEWS 26
         AUG 27
                 Full-text patent databases enhanced with predefined
                 patent family display formats from INPADOCDB
NEWS 27
         AUG 27
                 USPATOLD now available on STN
NEWS 28
         AUG 28
                 CAS REGISTRY enhanced with additional experimental
                 spectral property data
NEWS EXPRESS
              29 JUNE 2007: CURRENT WINDOWS VERSION IS V8.2,
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NEWS EXPRESS 29 JUNE 2007: CURRENT WINDOWS VERSION IS V8.2, CURRENT MACINTOSH VERSION IS V6.0c(ENG) AND V6.0Jc(JP), AND CURRENT DISCOVER FILE IS DATED 05 JULY 2007.

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=> s olefin and distillation

105038 OLEFIN 103696 OLEFINS

159968 OLEFIN

(OLEFIN OR OLEFINS)

58989 DISTILLATION

422 DISTILLATIONS

59144 DISTILLATION

(DISTILLATION OR DISTILLATIONS)

178561 DISTN

1798 DISTNS

179306 DISTN

(DISTN OR DISTNS)

197143 DISTILLATION

(DISTILLATION OR DISTN)

L1 4941 OLEFIN AND DISTILLATION

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PROPANE IS NOT A RECOGNIZED COMMAND
The previous command name entered was not recognized by the system.
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"HELP COMMANDS" at an arrow prompt (=>).
=> s propane and (propene or propylene)
         83136 PROPANE
          1129 PROPANES
         83715 PROPANE
                  (PROPANE OR PROPANES)
         75360 PROPENE
           775 PROPENES
         75697 PROPENE
                  (PROPENE OR PROPENES)
        190060 PROPYLENE
           305 PROPYLENES
        190159 PROPYLENE
                  (PROPYLENE OR PROPYLENES)
L2
         14686 PROPANE AND (PROPENE OR PROPYLENE)
=> s 11 and propane and (propene or propylene)
         83136 PROPANE
          1129 PROPANES
         83715 PROPANE
                  (PROPANE OR PROPANES)
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           775 PROPENES
         75697 PROPENE
                  (PROPENE OR PROPENES)
        190060 PROPYLENE
           305 PROPYLENES
        190159 PROPYLENE
                  (PROPYLENE OR PROPYLENES)
L3
           207 L1 AND PROPANE AND (PROPENE OR PROPYLENE)
=> s 13 and (epoxidation or epoxide)
         14673 EPOXIDATION
           245 EPOXIDATIONS
         14706 EPOXIDATION
                  (EPOXIDATION OR EPOXIDATIONS)
         26255 EPOXIDN
           570 EPOXIDNS
         26343 EPOXIDN
                  (EPOXIDN OR EPOXIDNS)
         28048 EPOXIDATION
                  (EPOXIDATION OR EPOXIDN)
         50076 EPOXIDE
         28851 EPOXIDES
         65150 EPOXIDE
                  (EPOXIDE OR EPOXIDES)
L4
            10 L3 AND (EPOXIDATION OR EPOXIDE)
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=> d 14 1-10 abs ibib

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ANSWER 1 OF 10 CAPLUS COPYRIGHT 2007 ACS on STN
Procedure; for the continuous recycling an off-gas flow containing an unreacted olefin resulting by oxidation of olefins with hydroperoxides, includes following steps (1) compaction and cooling the off-gas flow, (2) separation the olefin from the off-gas flow by distillation, and (3) epoxidn of the separated olefin with a hydroperoxide. The procedure is especially useful for epoxidn. of propene to propene oxide, whereby the off-gas flow contains propene and propene.

SSION MUNBER: 2004:367231 CAPLUS
LACINITY NUMBER: 140:357189
E: Procedure for the continuous recycling an unreacted olefin resulting by oxidation of olefins with hydroperoxides by compaction and pressure distillation

NT ASSIGNEE(S): BASF AG, Germany
CE: Ger. Offen., 6 pp.
CODEN: GWXXBX
MENT TYPE: Patent
ACCESSION NUMBER:
DOCUMENT NUMBER:
TITLE:
 PATENT ASSIGNEE(S):
SOURCE:
 DOCUMENT TYPE:
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DOCUMENT TYPE:	Patent						
LANGUAGE:	German						
FAMILY ACC. NUM. COUNT:	1						
PATENT INFORMATION:							
		APPLICATION NO.					
		DE 2002-10249378					
		CA 2003-2503449					
		WO 2003-EP11736					
		BA, BB, BG, BR, BY, BZ,					
		DZ, EC, EE, EG, ES, FI,					
GH, GM, HR,	HU, ID, IL, IN,	IS, JP, KE, KG, KP, KR,	KZ, LC, LK,				
LR, LS, LT,	LU, LV, MA, MD,	MG, MK, MN, MW, MX, MZ,	NI, NO, NZ,				
OM, PG, PH,	PL, PT, RO, RU,	SC, SD, SE, SG, SK, SL,	SY, TJ, TM,				
TN, TR, TT,	TZ, UA, UG, US,	UZ, VC, VN, YU, ZA, ZM,	ZW				
RW: GH, GM, KE,	LS, MW, MZ, SD,	SL, SZ, TZ, UG, ZM, ZW,	AM, AZ, BY,				
		BE, BG, CH, CY, CZ, DE,					
FI, FR, GB,	GR, HU, IE, IT,	LU, MC, NL, PT, RO, SE,	SI, SK, TR,				
BF, BJ, CF,	CG, CI, CM, GA,	GN, GQ, GW, ML, MR, NE,	SN, TD, TG				
		AU 2003-278127	20031023				
EP 1558596	A1 20050803	EP 2003-769439	20031023				
R: AT, BE, CH,	DE, DK, ES, FR,	GB, GR, IT, LI, LU, NL,	SE, MC, PT,				
IE, SI, LT,	LV, FI, RO, MK,	CY, AL, TR, BG, CZ, EE,	HU, SK				
CN 1705652	A 20051207	CN 2003-80101850	20031023				
MX 2005PA04183	A 20050608	MX 2005-PA4183	20050420				
US 2006058539	A1 20060316	US 2005-532096	20050421				
IN 2005CN00702	A 20070629	IN 2005-CN702	20050421				
PRIORITY APPLN. INFO.:		DE 2002-10249378	A 20021023				

WO 2003-EP11736

ANSWER 3 OF 10 CAPLUS COPYRIGHT 2007 ACS on STN An olefin is treated with an epoxidizing agent to give a mixture of an epoxide and a carboxylic acid by-product which is separated by a double extraction procedure. The mixture is partitioned using a

a double extraction processes. "In measurement insiscible with H2O, which dissolves the epoxide, and an aqueous solvent to dissolve and extract the acid. Thus, a mixture containing epoxide derivs. of Cl4 1-alkenes 34.3, AcOH 19, and EtoAc 46.73 was passed at 1660 g/hr into the conter of a 5 cm disseter 'York-Scheibel column with 20 stages, operating at 25°. Water (1.3 parts/l part AcOH) was introduced at the top of the column and 930 g/hr pentane at the bottom. The nonaq, phase withdrawn at the top contained 89% EtoAc and 0.6% AcOH while the aqueous phase at the bottom contained 39.4% AcOH and

EtOAc, which was separated by distillation A similar process was used to sep. a mixture containing AcOH, propylene, propane, EtOAc, and propylene oxide.

ACCESSION NUMBER: 1970:3346 CAPLUS
DOCUMENT NUMBER: 72:3346 /2:3346
Recovery of hydrophobic epoxide compounds
Taylor, Wallace Edmondson; Sehnert, Merle F.
Celanese Corp. INVENTOR(S):
PATENT ASSIGNEE(S):
SOURCE: Fr., 7 pp. CODEN: FRXXAK DOCUMENT TYPE: Patent French FAMILY ACC. NUM. COUNT: PATENT INFORMATION:

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE		
FR 1551419		19681227	FR	19680110		
DE 1643852			DE			
GB 1186333			GB			
US 3541114		19701117	US	19670113		
PRIORITY APPLN. INFO.:			us	19670113		

A continuous process for the epoxidn. of olefins (e.g., methyloxirane from propylene) with hydrogen peroxide using a product-stream predistn. step and unit is described and a process flow diagram presented. 2001:581493 CAPLUS ACCESSION NUMBER: DOCUMENT NUMBER: TITLE: 135:137842
Process for the epoxidation of olefins using a product-stream predistillation step and unit Hofen, Willi: Thiele, Georg; Moller, Alexander Degussa A.-G., Germany Eur. Pet. Appl., 10 pp.
CODEN: EPXXDW
Patent INVENTOR(S): PATENT ASSIGNEE(S): SOURCE: DOCUMENT TYPE: Patent LANGUAGE: LANGUAGE: FAMILY ACC. NUM. COUNT: PATENT INFORMATION: PATENT NO. KIND DATE APPLICATION NO. DATE

EP 1122248 A1 20010808 EP 2000-102544 20000207
R: AT, BE, CH, DE, DK, ES, FR, GB, GR, IT, LI, LU, NL, SE, MC, PT,

12 SI, LT, LV, FI, RO

MO 2001057010 A1 20010809 MC 2001-EP1166 20010203
W: AE, AG, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, BZ, CA, CH, CN,
CR, CU, CZ, DE, DK, DM, DZ, EE, ES, FI, GB, GD, GE, GH, GM, HR,
HU, ID, IL, IN, IS, JF, KE, KG, KF, KR, KZ, LC, LK, LR, LS, LT,
LU, LV, MA, MD, MG, MK, MN, MW, MC, MZ, NO, NZ, PL, PT, RO, RU,
SD, SE, SG, SI, SK, SI, TJ, TH, TR, TT, TZ, UA, UG, US, UZ, VN,
YU, ZA, ZW, AM, AZ, BY, KG, KZ, MD, RU, TJ, TM
RN: GH, GM, KE, LS, MN, MZ, SD, SL, SZ, LTZ, UG, ZM, AT, BE, CH, CY,
DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE, TR, BF,
BJ, CF, CG, CI, CM, GA, GN, GW, ML, MR, NE, SN, TD, TG
BR 2001008063 A 20021105 BR 2001-8063 20010203
EP 1254126 A1 20030702
R: AT, AT, BE, CH, DE, DK, ES, FR, GB, GR, IT, LI, LU, NL, SE, MC, PT,
AT 244231 T 20030715 AT 2001-91586 20010203
EP 1254126 B1 20030715 AT 2001-91586 20010203
ER 2002085104 T 20030715 JF 2001-516860 20010203
EA 2002005200 A 20030715 JF 2001-516860 20010203
EA 2002005500 A 20030715 JF 2001-516860 20010203
EA 2002005501 A 20030715 JF 2001-556860 200102 PATENT NO. A1 20010808 APPLICATION NO. DATE w 20010203 THERE ARE 4 CITED REFERENCES AVAILABLE FOR THIS RECORD. ALL CITATIONS AVAILABLE IN THE RE REFERENCE COUNT: FORMAT

ANSWER 2 OF 10 CAPLUS COPYRIGHT 2007 ACS on STN

ANSWER 4 OF 10 CAPLUS COPYRIGHT 2007 ACS on STN
The title compds. were prepared in a 2-step conversion process of
olefins which were gaseous under normal conditions with ACOON (1).
Thus, 1680 g. propylene (II) and 676 g. I (20% by weight solution in
ACOET were allowed to react per hr. in a 2-step reaction. The

AGOST were allowed to least parmit. In a coop state of the conversion in the last step took place at 50° in 50 mm. in diameter The conversion in the last step took place at 50° in 50 mm. and the 2nd step at 100° in 10 min.; in both steps the pressure was 100 atmospheric Unreacted II was recycled after condensation at 50°. The reaction product was passed to a distillation column and subjected to fractional distillation at atmospheric pressure. Propylene oxide (IIII), b. 33-5°, was removed at the top at 402 g./hr. 77.9° yield with respect to I supplied, and 77.1% with respect to the nonconverted II conversion was 22.5% by weight and I conversion was 95% by weight

use of Me2CO resulted in 362 g. III/hr. (70.1% with respect to II and 73% with respect to I). II conversion was 21.4% by weight and the I conversion

97% by weight. The following results were obtained with a U4A reactor:

. III/hr., III yield with respect to I, 69.5%. III yield with respect to II, 78%; I conversion, 98% by weight; II conversion, 19.8% by weight mount

mount of distillation residue was 0.3 kg./kg. III formed while 13% CO2 was formed with respect to 1 C atom of I. Corrosion gave 0.000% by weight

in the reaction mixture with respect to I solution (1.1 g./m2/ day).

experiment was carried out with 0.01% by weight Na5P3010 and 0.01% by

crupingline as stabilizers. The results were: 465 g. III/hr.; III yield with respect to I, 90.1%; with respect to II, 87.6%; I conversion 97% by weight; and II conversion 22.6% by weight Isobutylene (3420 g.) and 20%

I solution in EtOAc (4940 g.) was stabilized with 0.01% by weight Na5P3,010 and

0.01% by weight quinoline. The mol. ratio isobutylene-I was 4.7:1; in

the

lat step, the temperature was 30° and the time 30 min.; in the second step, temperature 70°, time 6 min. Pure isobutylene oxide was obtained (88.2 % with respect to I supplied).

ACCESSION NUMBER: 65:13342 CAPLUS DOCUMENT NUMBER: 65:13342 CAPLUS DOCUMENT NUMBER: 65:13656a-c
TITLE: Alkane epoxides
INVENTOR(S): Knapack, A.-G.
SOURCE: 11 pp.
DOCUMENT TYPE: Patent

Unavailable PAMILY ACC. NUM. COUNT: 1 PATENT INFORMATION:

PATENT NO. KIND DATE APPLICATION NO. DATE NL 6513640 BE 671268 19660425 NL 1965-13640 19651021 PRIORITY APPLN. INFO.: DE 19641022 (Continued)

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ANSWER 6 OF 10 CAPLUS COPYRIGHT 2007 ACS on STN cf. CA 57, 13716g. The (tert-Bu)202 (I)-induced free radical addition of propylene oxide (II), styrene oxide (III), 1,2-epoxybutane (IV), 1,2-epoxyoctane (V), and 1,2-epoxy-3-phenoxypropane (VI) to 1-octene
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was studied in the temperature range 125-200°. A mixture of isomeric epoxybutanes distilled gave 2,3epoxybutane, b. 56-7°, n2D0 1.3815, and IV. b. 58.5-9.0°, n2D0 1.3832. The base-catalyzed reaction of H2O with mestivel oxide according to Fayne (CA 52, 16357f) gave 4-methyl-3,4-epoxy-2pentanone (VIII), b2O 61-2°, n2D0 1.4235. V (2 moles), 0.40 mole VII, and 0.06 mole I deserated with N and heated 3 hrs. at 145°, the mixture freed from peroxide decomposition products and unreacted V and VII by distillation, the residue distilled at 0.10 mm. to remove the 1:1 adduct, and the product redistd. gave 7.7% 7-hexadecanone, b0.10 82°, n2D0 1.4432, X 5.88 u failing to give pos. ketone test with Brady reagent and HONNE.HCl, or to yield a marbazone.

ketone test with Brady reagent and HONHZ.HCl, or to yield a semicarbasene.

Gas-chromatographic comparison of its retention time with that of an authentic synthetic sample proved the assigned structure. IV (2 moles 0.40 mole VII, and 0.06 mole I heated 3 hrs. at 145 in a deserated Parr autoclave yielded 3.43 g. 3-dodecanone, b0.15 65 ', n200 1.4425, \$5.85, \$3.0 . III (2 moles) 0.20 mole VII, and 0.03 mole I heated 3 hrs. at 150 under Nand the mixture distilled gave 3.10 g. capriphenone (95% pure), b0.50 120-87, n200 1.4975, 5.85 . VI (1 mole), 0.10 mole VII, and 0.03 mole I heated 5 hrs. at 150 under N, the mixture distilled, and the solid (4.45 g., b1.0 170-200') recrystd. 4 times from petr. ether gave a product, m. 83', \$5.85, mol. weight \$27, consisting of 21 and 3:1 addition products (mol. weight 486 and 598). These results indicated that the chain transfer

sfer atom was the α-tertiary H atom on the epoxide ring.
Formation of this product also indicated that the intermediate epoxy radicals, initially formed, rearranged to α-oxo radicals before addition to the olefin. A mechanistic path for this general reaction was outlined and discussed. II (3 moles), 0.20 mole VII, and 0.015 mole I in a deserated steel bomb heated 17 hrs. at 125° and the mixture distilled gave 2.33 g. 5-hydroxy-2-hexanone (IX), 80% pure, 0.

) 60-90°, n2DO 1.4520, mol. wéight 120.7, Å 3.0, 5.85 µ, together with 2.33 g. residue, mol. weight 640. II (2 moles), 0.20 mole

and 0.03 mole I heated 2 hrs. at 150° in a descrated Perr bomb and the mixture distilled left a residue of 11.2 g., n2D0 1.4595, mol.

the mixture distilled left a residue of 11.2 g., n2D0 1.4595, mol. weight 324, and gave 5.34 g. product, b0.26 62-70*, n2D0 1.4368, mol. weight 211, \(\lambda 3.0, 5.85 \) \(\text{\mu}\), chromatographed to show the presence of 4.27 g. 1X and 1.07 g. 2-undecanone (X). II (2 moles), 0.10 mole VII, and 0.12 mole I heated 1 hr. at 200° in a deserated Parr bomb and the mixture distilled left 10.2 g. residue, n2D0 1.4622, mol. weight 349, and gave 1.25 moles (1.25 moles).

Product, b0.26 50-7*, n2D0 1.4370, mol. weight 175.6, h 3.0, 5.85 u, containing 0.96 g. IX and 3.84 g. X: X semicarbazone m. 118-20*. With II, a secondary reaction, involving opening of the epoxide ring by intermediate acetonyl radicals, produced IX. To exacertain the effect of ring size on the rate of H atom abstraction, the reactivities of the above epoxides II, III, IV, V, VI, VII as, well as trimethylene oxide, tetrahydrofuran, and tetrahydropyran toward Me3CO, radicals were determined relative to C6H6. The reactant and I in

molar ratio was weighed into a glass ampul cooled in a solid CO2-CHC13-CC14 bath, flushed with argon, the sealed ampul heated 40 hrs.

ANSWER 5 OF 10 CAPLUS COPYRIGHT 2007 ACS on STN
Olefins with more than 3 carbon atoms can be epoxidated in
liquid phase by molecular oxygen using as catalyst olefinic aldehydes,
that give the corresponding olefinic acids, and sulfur or aromatic nitro
derivatives. Thus: A solution of 168 g acrolein, 420 g, propylene
, 180 g. nitrobenzene, and 1170 g. EtoAc is poured into a pressure
al. and 28.4 g. 1,2-epoxypropane (90%). A solution of 112 g. acrolein, 420 g.

propylene, 1369 g. EtOAc, and 5 g. sulfur is heated at 80°, and treated with molecular oxygen 2 hrs. to give (with recyclization) 82% 1,2-epoxypropane, and 70% acrylic acid, without sulfur the yields are 15% and 70%, respectively. A solution of 210 g. methacrolein, 420 g. propylene, 180 g. mitrobenzene, and 1130 g. EtOAc is heated at 95° and treated with oxygen for 16 min. to give (with recyclization) 85% 1,2-epoxypropane, and 66% methacrylic acid, (conversions 7.6% and 26%, respectively). A solution of 210 g. crotonaldehyde, 420 g. propylene, 180 g. nitrobenzene, and 1130 g. EtOAc is heated at 90° and treated with oxygen for 25 min. to give (with recyclization) 91% 1,2-epoxypropane, and 65% crotonic acid (conversions 5.8%, and 66%, respectively).

ACCESSION NUMBER: 1965:471400 CAPLUS

BOUNCENT NUMBER: 63:71400 CAPLUS

G3:71400 CAPLUS

G SOURCE: DOCUMENT TYPE: LANGUAGE: FAMILY ACC. NUM. COUNT: PATENT INFORMATION: APPLICATION NO. KIND DATE DATE FR 1401176 PRIORITY APPLN. INFO.: 19650521

ANSWER 6 OF 10 CAPLUS COPYRIGHT 2007 ACS on STN (Continued) at 135 t 1 stirred oil bath), the cooled ampul opened, and the mixt. analyzed by gas chromatography. The reactivity studies were tabulated and results indicated that 5- and 6-membered cyclic ethers underwent H atom abstraction most readily. Trimethylene oxide, II, and Locurent Number: 1963:421224 CAPLUS
DOCUMENT NUMBER: 95:21244
DOCUMENT NUMBER: 59:21224
TITLE: Proposition of the proposition o

1963:421224 CAPLUS
59:21224
59:3748a, 3749a-f
Free radical chemistry of cyclic ethers. IV. Free radical rearrangement of spoxides
wallace, T. J.; Gratter, R. J.
Univ. of Connecticut, Storrs
Tetrahedron (1963), 19, 657-65
CODEN: TETRAB; ISSN: 0040-4020
Journal AUTHOR(S): CORPORATE SOURCE: SOURCE: DOCUMENT TYPE: LANGUAGE:

Journal Unavailable CASREACT 59:21224 OTHER SOURCE(S):

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ANSWER 7 OF 10 CAPLUS COPYRIGHT 2007 ACS on STN
The autoxidn. of allyl chloride (I), methallyl chloride (II),
1,4-dichlorobutene-2 (III), and 3,4-dichlorobutene-1 (IV) formed
chlorohydrine by attack at the double bonds. Analysis of the initial
products from II indicated an epoxide precuraor was involved.

Exidation rates for III and IV were studied and show an unusual
dependency on added anions. All allylic chlorides were fractionated. Oxidna. at
                  spheric pressure were conducted using cylinder o. For pressure oxidns, an autoclave was used. Products from I and II were snalyzed by gas chromatography. Without a catalyst the oxidation of II at 60° was very alow. A maximum oxidation rate of 5.5 + 10-7 mole 0/ mole olefin/sec, was reached in 12 hrs.; after 44.7 hrs. 0.064 mole of 0/mole II was consumed, and the reaction terminated. In order to obtain
                  higher conversion and allow isolation of products 90.6 g. II containing
                  cobaltic acetyl-acetonate and 5 g. cumene hydroperoxide oxidized 46.3
                 at 60° and distillation of an 89-g. aliquot of the liquid product gave 40.7 g., b200 35-7°, 5.9 g., b200 78-9° (contained 1.6 milliequiv. of epoxide), 2.5 g., b50 55-75°, 4.5 g. b10 66-90°. At 200 lb./sq. in. 487.1 g. II containing 20 g. MgO and 4.8 g. tert-butyl hydroperoxide oxidized at 100° with an off gas, the reaction terminated at 375 min. after the consumption of 3.55 moles of 0, the solid product separated, dissolved 20.
                     o,
washed, acidified, and extracted with Et2O gave 9.8 g. of liquid
                  mainly of HCO2H. The 510 g. of liquid oxidation product gave a min. of
15

separate peaks on gas chromatography. Chloroacetone and 1,3 - dichloro 2 - methylpropenol-2 (Y) constituted 24 and 11%, resp. Chloroacetone an 1,2-epoxy-3-chloro-2-methylpropene (VI) were identified by infrared gas spectra. V was purified by rediatin, bl4 62.8*, n200 1.4700, d20
1.250. The bis-2-naphthyl ether derivative m. 146-8*. Reaction with aqueous suspension of Ca(OH)2 gave VI. Acidification of the salts yielded
                ded nearly all HCO2H, a trace of AcOH, and no chloroacetic acid [43.2 min.]. Attempts to titrate samples from various reaction stages for operoxide odometrically gave poor results. I [497.3 g.] containing 20 g. MgO at 100° and 200 lbs./aq. in. for 440 min. required 76.8 g. O and a constant maximum rate was reached in 260 min. CICH2CHO was identified.
                  was present in the distillate. 1,3-Dichloropropanol was isolated as a pure liquid; phenylurathan m. 172-3°. The acid components (8.5 g.) extracted from the acidified MgO contained equal amts, of chloroacetic
and HCO2H. The oxidation of III at 90° was terminated after the consumption of 0.74 mole O at 27 hrs. Several tenths of a gram of (CO2H2)
(CO2M2)

Was directly filtered. The solution was found to contain 2.2

milliequiv./g.

of acid. The solution, 81 g., taken up in CHC13, washed, dried, and
distilled.
of acid. The solution, 81 g., taken up in CRC13, washed, dried, and distilled gave 13 g. unchanged III. No 1,3-isomer was obtained. Trichlorobutanol
                  28% yield was collected at 68-77^{\circ}/1 mm., n25D 1.4980. The oxidation of 2M III in AcOH with 0.1M cobaltous chloride gave 0.19 mole HCl and
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GI For diagram(s), see printed CA Issue.

a cf. C.A. 50, 24121. Me2CHC(OH)Ph2 (I) gave 60% Mc2C:CPh2 (II) with Ac2O

and 50% with o-C6H4(CO)2O (IIa); it was best prepared by keeping 40

g. I, 50 g. C5H5N, and 42 g. POC13 at room temperature several days,
pouring on
pouring on
ice, extracting with Et20, drying the exta., concentrating, distilling,
refluxing the
distillate 6 hra. with Na, and redistg. to give pure II, bl.6 ll4°,
n23.50 l.586. II (20 g.) in 100 cc. Ac20 treated in 0.5 hr., with
cooling, with 15 g. Cr203 in 80 cc. Ac20, stirred 3 hrs., poured into 1.5
l. H20, and the product extracted with Et20 gave 14.4 g. CMe2.CPh2.0
(III).
                1. H20, and the product extraction and the reaction were identified as Ph2CO and Me2CO. II and Bz2O2 also gave III, b0.25 88°. III (0.2 g.) and 5 cc. 43% H2SO4 shaken several days gave a diol, m. 94-5° (petr ether). II reacted vigorously with Cr2O3 in 65% H2SO4, giving no III, but instead, Ph2CO and Me2CO. PheC6H4CH(OH)CHMe2 and saturated Et2O-HC1 gave p-MeC6H4CHCHCHMe2 which, treated in situ, with CSHSN gave p-MeC6H4C:CMe2 (IV), m. 58-9° (alc.). As above, 20 g. IV and 11 g. Cr2O3 in A2O2 gave 13 g. epoxide (V), b1.5-1.7 139-42° (by-products were (p-MeC6H42CO and Me2CO); IV and Bz2O2 also gave V, m. 58-9°. V, as above gave a diol, identified by oxidation with HIO4 to (p-MeC6H4]2CO (VI). IV and Cr2O3 in 43% H2SO4 gave VI but no V. p-BrC6H4MgBr (from
                  g. p-BrC6H4Br and 60 g. Mg) and 110 g. Me2CHCO2Et gave crude (p-BrC6H4)2C(OH)CHMe2 (VIII); distillation of VII gave (p-BrC6H4)2C(CM2 (VIII); bd. 7174*, m. 97* (alc.); as above, 15 g. VIII gave 10 g. epoxide (IX), bl.2 177-8*, m. 94-5* (alc.); IX was unaffected by 43* H2504 at room temperature for 3 days. Similarly were prepared (p-ClC6H4)2C(OH)CHMe2, (p-ClC6H4)2:CMe2,
   DO.2

132', m. 71-2', and the epoxide (X), b0.65

148-50', m. 57-8'. Me2CHCHMeC(OH)Ph2, b2 198-200',
n170 1.564, (205 g.) and 600 g. 118 gave Me2CHCHe:CPh2 (XI), b15

168-70', n150 1.5740 and X gave the epoxide (XII), b12

172-4', m. 93' (alc.), XII also resisted hydrolysis with 43%

H2304. Me(iso-Pr)C(COZEL)2 gave Me2CHCHMeCO2H, b. 142-6', n20D

1.4023.

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POCUMENT NUMBER: 52:25393 CAPLUS
 DOCUMENT NUMBER:
ORIGINAL REFERENCE NO.:
                                                                                         52:4561g-i,4562a-b
Reactions of unaaturated compounds. XIII. Oxidation
                                                                                         l,l-dierylolefins by chromic oxide
Hickinbottom, N. J., Moussa, G. E. M.
Univ. London
Journal of the Chemical Society (1957) 4195-8
CODEN: JCSOA9; ISSN: 0368-1769
 AUTHOR(S):
CORPORATE SOURCE:
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LANGUAGE:
                                                                                          Unavailable
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mole CO2/mole of III. Distn. gave no sepn. of products. An 82% yield of a liquid b3 73-160° consisted of esters conteminated with acids, olefinic, and hydroxy compds. Titration of the crude oxidn. mixt. for hydroperoxide was unsuccessful. Oxidn. of IV at 90° with 0.5% Co naphthenate consumed 0.16 mole 0 in 24 hrs., and purification of the product gave 35 g. IV and 7.6 g. III. No isomer was recovered for reaction in the absence of catalyst. The combined products from oxidn.

Of

M IV in AcOH representing 225 g. starting material were distd. The AcOH forerun of 29 g. yielded an unatable 2,4-dinitrophenylhydrazone, m. 125°. From the 18.5 g. fraction, b4 36.6°, 4.5 g. crystals were obtained, m. 62-3°, probably CICH2CO2H. The p-bromophenacyl ester m. 97-9°. The ester fraction, b4 72-81°, 14.5 g. on hydrolysis with 18 H2504 and ateam distn. gave AcOH and a liquid from which 1,2,3'-4-teria-chlorobutane was obtained as platelets, m. 73°. The remaining liquid was trichlorobutanol; urethan m. 112-3°. The next highest boiling distillate, b18-127°.

B.6 g., appeared to be a mixt. of esters. And the last fraction of 17 g.

b1.1 127° pptd. some crystals, m. 76-7°. The pot residue was 40.8 g. Pure 1,3'4-trichlorobutanol-2 (VII) was obtained by refluxing either the impure chlorohydrin or the ester fraction from the oxidn. of III or IV with 5 times its wt. of N MeOH-HCl. VII bl 80°, n250 1.5022.0 With base VII gave an epoxide, b44 96-100°, n200 1.4749; phenylurethan m. 132-3°. Reaction of the chlorohydrin with 201 MaOH gave 804 dichloroepoxybutane, bl0 73-5°, n200 1.4767. The rate of basic hydrolysis of 0.1N chlorohydrin was second order rate. A plot of O consumed against time generally produced typical sigms shaped curves. The following results were obtained (isomer, solvent, temp.. concn. of the dichlorobutene, conen. of catalyst, added salt or acid, and the rate + 104 giveni: IV, AcOH, 90°: 2M, 0.1M, CoOAc, 10; M, 0.5M, coOAc, 7.6; 2M, 0.05M, coOAc, 7.6; 2M, 0.05M, coOAc, 7.6; 2M, 0.05M, coOAc, 7.6; 2M, 0.05M, coOAc, 7.6; 2M
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AB Epoxides are prepared by treating an ethylenically unsatd. compound with AcH- or EtCicio-monoperacylate, preferably at 40-120°. Thus, 351 g, of a mixture of AcH (751) and Me2CO (253) charged to a cylindrical oxidizer, cooled to -4°, irradiated with ultraviolet light, and O forced through by means of a diffuser gives 46% AcH-monoperacetate (1) at the end of 2 hrs. Fresh AcHMe2CO may be added at the top of the oxidizer and the oxidized product removed from the bottom. Styrene (413 g.) containing

O.8 g. 4,26-Cl(O2N)2C6H2OH (II) is charged to a still, refluxed at 70° under 60 mm. pressure, 229 g. of a 52% solution of I (prepared as above) added over a period of 80 min. and 10% II in styrene is added simultaneously through the reflux column at a rate of 20 ml./78 min. and the AcOH, Me2CO, and AcH are removed continuously. Distillation of the residual material gives 86 g. styrene oxide, as well as unreacted styrene. Similarly were prepared the following from the corresponding olefins: 4-vinyleyclohexen monoxide, b9 57°; propylene oxide, 3,4-epoxy-4-methyl-2-pentanone, b26 65°; 9,10-epoxystearic acid, m. 52°; glyridol, b5 57°; chloroisobutylene oxide, b50 46°; butadiene monoxide; 3,4-epoxyeyclohexanear-bonitrile, b2.5 76-85°; 9,10-epoxystatice-examide: N-(n-butyl)-4,5-epoxyeyclohexanear-bonitrile, b2.5 76-85°; 9,10-epoxystatice-examide: N-(n-butyl)-4,5-epoxyeyclohexanear-lowinde.

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L4 ANSWER 10 OF 10 CAPLUS COPYRIGHT 2007 ACS on STN AB The object of this work was the preparation and study of the phys. properties

erties
of certain hydrocarbons with b. ps. in the range of gas oil (petroleum)
fraction b. 200-320°. Preparation of hydrocarbons: Aliphatic series: (1)
Pentadecane (1). Condensation of (CR20)3 with C6H13Mpsr gave 38%
heptanol; condensation of C7H15MpBr with HC02Et gave 61% 8-pentadecanel
(11), m. 43.5° (from EtoH-H20), bll 153° (cf. C.A. 41. 58504)
for data on C6H13Br and C7H15Br). Dehydration of II in H2504 gave
7-pentadecene, b20 137°, d20 0.7726, n20D 1.4370, MR (mal.
refraction) 71.21, oxidation of which with Cr03-H0Ac yielded heptanoic

b. 218-24°, and octanoic acid, b. 233-8°, both characterized by titration and the Ag salts. Catalytic hydrogenation with Pt black of

gave I, b22 145°, d20 0.7638, n20D 1.4286, MR 71.49. (2) 4,6-Dipropylnonane could not be prepared The 4-heptanol (III) prepared

8% yield from C3H7MgBr and HCO2Et b25 70°, d20 0.8127, n20D 1.4184, MR 36.00; these data compared favorably with those for III prepared from C3H7MgBr and C3H7CHO, in contrast to the poorer data for III prepared

esters: b25 64*, d20 0.8139, n20D 1.4181, MR 35.92. The C7H15MgBr was formed with difficulty, BtBr being necessary to prime the reaction, and subsequent condensation with HCOZEt gave only secondary products, notably 2-propyl-1-pentanol. The preparation of 3-propyl-2-(2-propylbutyl)hexanoic acid (IV) by malonic ester synthesis (for subsequent decarboxylation to C15H32) was unsuccessful. (3) 2,4.8,10-Tetramethylhendecane could not be prepared from MeZCHCHZCHMeCHZMgBr and HCOZEt; only secondary products were obtained. 4-Methyl-2-pentanol, 81% from MeZCHCHZMgBr and AcH, b10 47*, d20 0.80708, n20D 1.4101, MR 31.22; formation of its bromide with P and Br or with HBr was difficult, and subsequent condensation with (CH2O1) gave mostly secondary products and 88 2,4-dimethylpentanol. (4) 2,6-Dimethyl-3,5-diisopropylheptane was not formed from (MeZCH)ZCHZMP and HCOZET, but instead (MeZCH)ZCHZM MeZCHCH:CMe2, and (MeZCH)ZCHCHCMOR the considered improbable after attempted preparation of IV.

Hexadecane (V), 60% from 1-bromooctane and Na, bl1 153°, d20 0.7770, n20D.1.4351, MR 75.91; in 8t20 the reaction is slow, with an intermediate blue color; if 1-bromooctane is added to a suspension of Na in xylene, the initially fast solution of the Na is followed by the slow elimination of Br as NaBr (refluxing 3 h.) (70% yield). (6) 5-Methyl-4,6-dipropylnonane. The intermediate (Pr2CH)2C(OH)Me could not be obtained by Grignard condensation, only secondary products such as 3-propyl-2-hexanol. (7) 4,7-Dipropyldecane (VI). 4-Heptanone (VII),

4-heptanol and CrO3-HOAc, b741 142°, d20 0.8116, n20D 1.4065, MR 34.53; semicarbazone m. 135°. BrMgC.tplbond.CMgBr (VIII) was made by passing a stream of pure C2H2 into Et2O and EtMgBr until C2H6 evolution

ucion

ceased and 2 liquid layers appeared; condensation with VII gave 89%
acetylenic glycol, m. 120° (from CC14), dehydration of which in
boiling 25% HZSO4 gave 4,7-dipropyl-3,7-decadien-5-yne (IX), b25
142°, d20 0.8111, n200 1.4862, MR 77.19 (an extraordinary
exeltation of 4.04 was noted). Hydrogenation with Pt black gave VI with
phys. data different from those found in the literature (cf. C.A. 8,
1579), b23141°, d20 0.7802, n200 1.4350, MR 75.59. Selective
hydrogenation with Raney Ni in BtON gave instead intermediate products,
identified by oxidation: 4,7-dipropyl-3,5,7-decatriene, 4,7-dipropyl-4,6decadiene, and 4,7-dipropyl-5-decene. (8) 2,4,6,8,10-

ANSWER 10 OF 10 CAPLUS COPYRIGHT 2007 ACS on STN (Continued) 1,2-diphenyl-2-propanol, m. 72° (from EtOH), b9 163°, dehydrated in boiling 50% H2SO4 to 1,2-diphenyl-2-propene, m. 81° (from EtOH), b22 170°, slightly sol. in Et20.

Hydrogenation with Pt black was selective, to form XXI, b25 160°, d20 0.9799, n200 1.5573, XR 64.42. (4) 1,3-Diphenylpropane (XXII). PhCH2MgCl and HCO2Et gave only 7-8% 1,3-diphenyl-2-propanol (XXIII),

to the formation of secondary products such as PhCH2CH2OH; the Grignard condensation of PhCH2CH2DF with BzH gave 351 1,3-diphenyl-1-propanol (XXIV), m. 71° (from EtOH), bl4 186°. Dehydration of XXIII with H2SO4 gave trans-1,3-diphenylpropene, m. 51° (from EtOH), b25 159°; similarly XXIV gave a mixt., b15 170°, d20 0.9978, n20D 1.569, MR 63.68; chilling removed 30° as the solid trans form, and the oily liq. was purified to cis-1,4-diphenylpropene, b18 178°, d20 1.0138, n20D 1.5807, MR 63.75. XXII, formed by hydrogenation with Raney Ni of either isomer, b18 160°, d20 0.9931, n20D 1.5594, MR 64.41. (5) 1,2-Diphenylbutane (XXV), b28 172°, d20 0.9737, n20D 1.5554, MR 68.98. Friedel-Crafts condensation of EtCOCl and C6H6 gave

1.5554, MR 66.98. Priedel-Crafts condensation of EtCOC1 and C6H6 gave

Et Ph ketone, bll 97', d20 I.0103, n20D 1.5256, MR 40.69, which
with PhCH2MgC1 gave 1,2-diphenyl-2-butanol, b20 180', d20 1.036',
n20D 1.5752, MR 72.06. Dehydration in H2S04 or P205 gave a mixt. of
isomeric clefins: subsequent hydrogenation with Raney Ni was
selective, to form XXV, attacking only isomers without a double bond
between the 2 rings (the formation of XVIII from stilbene is an exception
to this general rule). (6) 1.4-Diphenylbutane (XXVII). The 2
disaterecisomers of 1.4 diphenyl-2-butyne-1,4-diol, from B2H and VIII,
were sepd. by their different solubilities in Et20; on crystn. from EtOH
the u-form m. 146' and the β-form m. 99.5'. The
products, predominantly u-, resinify easily in acid. Hydrogenation
gave the stereoisomeric diols; α-form (XXVII) of
1,4-diphenyl-1,4-butanediol m. 110'; β-form m. 93'. In
contrast to the aligh. diols, dehydration of XXVII with 30t H2S04 did not
give a diolefin, but instead 1,4-diphenyl-1,4-epoxybutane
(2,5-diphenyltetrahydrofuran) (XXVIII), b27 210', 420 1.0752, n20D
1.5770, MR 63.49, very stable, resistant to H in EtOH with Raney Ni or Pt
black, reacts slowly with H and Pt black in HOAc. In contrast, the
on

black, reacts slowly with H and Pt black in HOAC. In contrast, the on of nascent H, from Na and EtOH, is very effective, giving 1,4-diphenyl-1-butenol, b32 218*, d20 1.0347, i200 1.555, MR 65.17, dehydration in 604 H2SO4 then gave 1,4-diphenyl-1-butene, b14 170*, d20 1.0310, n200 1.5959, NR 68.37. The XXVI produced by hydrogenation with Raney Ni, m. 52.5*, was identical with that prepd. from PhCH2CH2R and Na. No rearrangement occurred in the dehydration of XXVII (cf. Tiffeneau, Orekhoff, and Levy, C.A. 26, 2429). (7) 1,2-Diphenylpentane (XXXIX), b32 184*, d20 0.9649, n200 1.5480, MR 73.74. 1,2-Diphenyl-2-pentanol, 944 from PhCH2CHGCl and PFB2, b22 184*, d20 0.9913, n200 1.5882, NR 81.50, was dehydrated with H2SO4 to a mixt. (XXXI) of isomeric clefins, b27 185*, d20 0.9958, n200 1.5798, NR 74.85*, dehydration with P2O5 gave a mixt. (XXXI), b28 196*, d20 1.0026, n200 1.5807, MR 73.76. XXXI contains mostly 1,2-diphenyl-2-pentene and is smoothly hydrogenated at normal pressure with Raney Ni to XXIX, whereas XXX, contg. mostly 1,2-diphenyl-1-pentene, is not hydrogenated. (8) 2,5-DiphenylHaene (XXXII). 2,5-Diphenyl-3-hexyne-2,5-diol, from VIII and MeBz, was sepd. into the a-form, m. 163.5* (from EtOH), and the predominant R-form (XXXIII) a. 126* (from C6H6), by the virtual insoly, of the a-form in EtO. Attempted dehydration caused resin formation, eap. with XXXIII and 101 H2SO4, when a red resin was obtained. So hydrogenation gave 2,5-diphenyl-2,5-hexanediol as the a-form

ANSWER 10 OF 10 CAPLUS COPYRIGHT 2007 ACS on STN (Continued)
Pentamethylhendecame. An attempted prepn. by Grignard condensation of
Me2CHCH2CHMcCH2Br with EtoAc gave only secondary products, such as
2,4-dimethyl-6-hexanol, 2,4-dimethyl-1-pentene, and 2,4-dimethylpentame.
(9) 2,4,6-frimethyl-3,5-diisapropylheptame could not be prepd. by

Me2CHCH2CHMCH2P with BtoAc gave only secondary products, such as 2.4-dimethyl-6-hearonl, 2.4-dimethyl-1-pentene, and 2.4-dimethyl-pentane. (9-2.4.6-Trimethyl-3,5-dimethyl-1-pentene, and 2.4-dimethylpentane. (9-2.4.6-Trimethyl-3,5-dimethyl-1-pentene, and 2.4-dimethylpentane. (9-2.4.6-Trimethyl-3,5-dimethyl-3,5-dimethyl-3,6-dimeth

ANSWER 10 OF 10 CAPLUS COPYRIGHT 2007 ACS on STN (Continued)
(XXXIV), m. 158.5°, and the B-form, m. 136°,
dehydration of XXXIV in 208 H2S04 gave (as with XXVII above).
2,5-diphenyl-2,5-epoxyhexene (2,5-dimethyl-2,5-diphenyl-terahydrofuran)
(XXXV), b29 202°, d20 1.0380, n20D 1.5637, MR 73.2°). The
resistance of XXXV to catalytic hydrogenation was analogous to that of
XXVIII, rupture of the heterocyclic ring with Na and EtOH gave
2,5-diphenyl-2-hexanol, b20 202°, d20 1.0125, n20D 1.5468, MR
74.52. Dehydration with 504 H2S04 gave 2 olefins: a solid form,
m. 138° (from EtOH), and a liq., b12 183°, d20 0.9916, n20D
1.5659, MR 77.62 (possible stereoisomers of 2,5-diphenyl-2-hexane) [cf.
Klages, Ber. 35, 2633(1902), and C.A. 1, 3005]. Attempted hydrogenation
of these olefins with Raney Ni did not form the desired XXXII,
but instead cyclization gave trans-1,2-dimethyl-1,2-diphenylcyclobutane
(XXXVII), b16 172°, m. 52.5°, and the cis-form (XXXVII), b16
172°, d20 0.9961, n20D 1.5540, MR 75.93; this reaction will be
investigated further with larger amts. of starting material. (9)
1,1,2-Triphenylethanel (XXXVIII). Dehydration of Ph2C(OH)CH2Ph
(triphenylethanel) (821 from Ph3E and PhCH2MgCI, m. 89°) with AcCl
gave Ph2C:CHPh, triphenylethylene, m. 73°, and hydrogenation with
Na and AmoH then gave the desired XXXVII, m. 54.5°. Cyclic
series: (1) Decylcyclohexane (XXXXII). Catalytic hydrogenation of
phenyldecane, 108 from 1-bromodecane, C666, and AlCl3, b14 150°,
d20 0.8978, n20D 1.5078, MR 72.36, with Pt black was strongly inhibited,
apparently by traces of AlCl3. BXH and C9H18 were also
ted.
Dehydration with H2S04 gave 1-phenyl-1-decene, b26 183-4°, d20

ed.
Dehydration with H2804 gave 1-phenyl-1-decene, b26 183-4*, d20
0.8726, n20D 1.4878, MR 71.29, hydrogenation of which then gave the
desired XXXIX, b20 168*, d20 0.8167, n20D 1.4520, MR 73.98. The
hydrogenation was selective, the intermediate phenyldecane being insol.

HOAc; the reaction then continued at 25% of the original rate. (2) 1,4-Diphenylcyclohexane could not be formed from C5Hill and p-Br2C6H4

Na; only C5H12, C5H10, C10H22, and dimethyloctane were formed. The condensation of C5H11MgBr with p-BrZc6H4 with FeCl3 (cf. C.A. 39, 2739.4 was also unsuccessful. (3) 1,2-Dicyclohexylethane (KI), obtained by the hydrogenation at 180' with Reney Ni of PhoRiZCH(0HPh), bl9 140', d20 0.8925, n20D 1.4802, MR 62.47. (4) 1,1-Dicyclohexylpropane (KII), from PhzCRCHZCHZOH by hydrogenation with Raney Ni, bl4 131', d20 0.9023, n20D 1.4935, MR 67.05. Condensation of EtCOZEt and C6H1MgCl gave only secondary products: 2. with

Condensation of ECCOZEL and CGH1MgCl gave only secondary products: 2.
C6H10, C6H11CH2AG, and cyclohexylpropanel. (5) 1,2-Dicyclohexylpropane (XLIII), from the hydrogenation of PhCH2CHPhMe with Pt black, b15 148*, d20 0.8819, n20D 1.4791, MR 66.90. (6) 1,3-Dicyclohexylpropane (XLIII), from the hydrogenation of PhCH2CH:CHPh in HOAc with Pt black, b24 151*, d20 0.8740, n20D 1.4790, MR 67.01; the hydrogenation was nonselective, acting equally on the olefinic bond and the arom. nuclei. (7) 1,2-Dicyclohexylbutane (XLIV), obtained from PhCH2C(OH)PhEt by hydrogenation with Raney Ni at 188*, b22 160*, d20 0.9146, n20D 1.5038, MR 71.85. (8) 1,4-Dicyclohexylbutane (XLIV), obtained similarly from [CH2CH(OH)Ph]2 at 180*, b19 161*, d20 0.8731, n20D 1.4758, MR 71.69, (9) 1.2-Dicyclohexylpentane (XLVI), btsined similarly from [CH2CH(OH)Ph]2 at 180*, b19 161*, d20 0.8731, n20D 1.4758, MR 71.69, (9) 1.7-Dicyclohexylpentane (XLVII), prepd. similarly from PhCH2C(OH)PhPr, b17 157*, d20 0.9218, n20D 1.5092, MR 76.47. (10) 2,5-Dicyclohexylmexane (XLVII), from (CH2C(OH)PhHe)2, b32 201*, d20 0.8901, n20D 1.4876, MR 80.87. (11) 1,1,2-Triphenylethanol was hydrogenated to 1,1,2-tricyclohexylethane (XLVIII), b30 230*, d20

ANSWER 10 OF 10 CAPLUS COPYRIGHT 2007 ACS on STN (Continued) 1.0236, n20D 1.5786, MR 90.21. Studies of hydrocarbon properties as a function of mol. structure: Generally the allph. hydrocarbons show increasing d. and n with increase in branching; the b. ps. decrease. The polyplefinic hydrocarbons show a trend in d. and n with the C/H ratio or degree of unsath. The mol. exaltation due to the acetylenic group is roughly 3 times that for ethylenic bonds. The following phys. data (see also under each of the preceding individual syntheses), i.e., the mol. exaltation (obsd. mol. refraction - calcd. value), the kinematic soit

onicy nitroles, and the abs. viscosity in centipoises, are given: XVII, in centistokes, and the abs. viscosity in centipoises, are given: XVII, -0.42, 3.45, 2.66; I, -0.01, 3.75, 2.35; V, -0.21, 4.33, 3.37; VI, -0.53, 3.71, 2.90; IX, -0.34, 4.65, 3.71; XI, -0.12, 10.28, 8.14; XII, -0.08, 9.64, 7.60; for the following only the mol. exaltation is given: IX, +4.04; XI, +4.19; XIV, +4.11; 5,8-dibuty1-4.6,8-dodecatriene, +2.02; 5,8-dibuty1-5,7-dodecadiene, +1.01; XVI, +4.28; 2,9-dimethy1-4,7-disobuty1-3,5,7-decatriene, +2.16; 2,9-dimethy1-4,7-disobuty1-4,6-decadiene, +1.02. The phys. state of the arylaliph hydrocarbons is intimately bound to the mol. structure esp. the degree of symmetry.

compds. are liq. whereas the sym. ones are solid. The d. and n of liqs. decrease with increasing chain length (or decrease in C/H ratio) and with increasing degree of symmetry. Phys. data (read as above): XIX, +0.18, 5.07, 5.06: XXI, +0.12, 6.74, 6.61; XXII, +0.15, 7.81, 7.83; XXV, +0.06, 9.36, 9.15; XXIX, +0.20, 12.00, 11.58. With the cyclic hydrocarbons, the d. and n of the sym. isomers are lower than of the asym. ones. Phys.

(read as above): XXXIX, +0.05, 6.14, 5.01; XL, -0.01, 7.90, 6.96; XLI, -0.05, 9.68, 8.74; XLII, -0.20, 11.52; 10.16; XLIII, -0.09, 8.91, 7.80; XLIV, +0.13, 10.99, 10.05; XLV -0.03, 12.71, 11.17; XLVI, +0.13, 14.68, 13.53; XLVII, -0.09, 23.35, 20.79; XLVIII, 0.00, 122.85, 127.80; XXXVI

\$2.5°, bl6 166°; XXXVII, bl6 172°, -0.03, 41.56,
41.40. The viscosity of the 3 series above at 20° increases with
the length of C chain, but not with the C/B ratio; the arylaliph, asym.
hydrocarbons have lower values than the corresponding cyclic compds. An
increase occurs with the appearance of closed rings, also with degree of
symmetry for compds, of snalogous structure. More evidence is needed to
confirm these generalities. Conclusions: (1) The Wurtz reaction does not
go so simply as given in the std. texts; free radicals play an important
part. Temp, is important, esp. in the isomerization of the radicals, and
it is difficult to isolate pure products, due to secondary products. (2)
The Grignard condensation is a better method for obtaining the desired
structures, with min. rearrangement of the reactants. (3) Dehydration

structures, with min. rearrangement of the reactants. (3) Dehydration and dehydrogenation depend greatly on mol. structure; the acetylenic diols dehydrate differently in the aliph. and arylaliph. series. After removal of the triple bond, spoxides are formed. Compds. of the type ArCH:CRAr are resistant to catelytic hydrogenation, so that selective redn. to arylaliph. or to cyclic hydrocarbons can be accomplished. Similarly, acetylenic diols are also selectively hydrogenated; the partial redn. of the triple bond is characterized by (1) a slower reaction, (2) change from exothermic to endothermic reaction, and (3) pptn. of the insol. olefin from EtOH. The hydrogenation of the sym. diaryl 1.4-epoxides is free of intromol. rearrangement.

ACCESSION NUMBER: 1948:27393 CAPLUS
DOCUMENT NUMBER: 1948:27393 CAPLUS
DOCUMENT NUMBER: 42:27383
ORIGINAL REFERENCE NO.: 42:58351-i,58364-i,5836a-i,5837a-i,5838a-e
Aliphatic, arylaliphatic, and cyclic (C14-C20) hydrocarbons. Synthesis

L4 ANSWER 10 OF 10 CAPLUS COPYRIGHT 2007 ACS on STN (Continued)
AUTHOR(S): Tuot, Marcell Guyard, Marcelle
CORPORATE SOURCE: Ecole natle. superieure petrole, Strasbourg
SOURCE: Bulletin de la Societe Chimique de France (1947)

1086-96 CODEN: BSCFAS; ISSN: 0037-8968

Journal Unavailable

DOCUMENT TYPE: LANGUAGE:

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5734 COMPRESS

(COMPRESS OR COMPRESSES)

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ANSWER 1 OF 8 CAPLUS COPYRIGHT 2007 ACS on STN A low-pressure olefins recovery process and plant are described in which feed gas is compressed and distilled at a primary distillation pressure. The overhead stream is chilled at <30 kg/cm2 to partially condense the overheads. The primary distillation tower is refluxed with at least a portion of the condensate. The overhead vapor
```

further chilled and partially condensed and the condensate is fed to a demethanizer. The remaining vapor is cooled in a cold section and the resultant liquid is phase separated and expanded to provide igeration for the cold section. The expanded vapor from the cold section is recycled

the process gas compressor. The bottoms streams from the primary distillation zone and the demethanizer are fractionated into resp. streams consisting essentially of ethylene, ethane, propylene, propane, C4's, and C5's. Process flow diagrams are presented.

ACCESSION NUMBER: 2006:8427 CAPLUS

DOCUMENT NUMBER: 144:88707

INVENTOR(S): Low-pressure olefin recovery process

Verma, Vijender K.; Hu, Jichuan

Kellogg Brown & Root, Inc., USA

U.S. Pat. Appl. Publ., 19 pp.

CODEN: USXXCO

DOCUMENT TYPE: Patent

DOCUMENT TYPE: LANGUAGE: English

FAMILY ACC. NUM. COUNT: PATENT INFORMATION:

	PAT	ENT	NO.			KIN	D	DATE		AP	PLICA	TION	NO.		D	ATE	
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	US	200	6004	242		A1		2006	0105	US	2004	8846	59		2	0040	702
	CA	249	7943			A1		2006	0102	CA	2005	2497	943		2	0050	222
	IN	200	5K00	0152		A		2007	0202	IN	2005	KO15	2		2	0050	310
	EP	163	7577			A2		2006	0322	EP	2005	-5372			2	0050	311
		R:	AT	, BE,	ÇH,	DE,	DK,	ES,	FR,	GB, G	R, IT.	LI,	LU,	NL,	SE,	MC.	PT.
			IE	, SI,	LT,	LV,	FI,	RO,	MK,	CY, A	L. TR.	BG,	CZ,	EE,	ΗU,	PL,	SK.
			BA	, HR,	IS,	YU											
	CN	171	5260			A		2006	0104	. CN	2005	1008	2196		2	0050	701
	MX	200	5 PAO	7272		A		2006	0111	MX	2005-	PA72	72		2	0050	701
RIC	RIT	AP	PLN.	INFO	. :					US	2004-	8846	59		A 2	0040	702

ANSWER 3 OF 8 CAPLUS COPYRIGHT 2007 ACS on STN

AB The process of U.S. 2,-600,110 (CA 46, 8358h), which is based on the heat-pump principle, is improved by passing a major portion of the compressed vapors of the kettle product refrigerant to the kettle section of the fractionator and compressing the rest of the vapors in a 2nd compression step so that they are condensed by available cooling water, thus increasing the efficiency of heat transfer. The improved process is particularly adapted to the separation of C2H4 from C2H6, C3H6 from C3H8, and C4H8 from C4H10.

ACCESSION NUMBER: 1966:57911 CAPLUS

DOCUMENT NUMBER: 64:57911

ORIGINAL REFERENCE NO.: 64:10793d-e

TITLE: Fractional distillation

INVENTOR(S): Palen, Joseph W.; Moon, John J.

PATENT ASSIGNEE(S): Phillips Petroleum Co.

5 pp.

5 pp. Patent Unavailable DOCUMENT TYPE: LANGUAGE:

LANGUAGE: FAMILY ACC. NUM. COUNT: PATENT INFORMATION:

APPLICATION NO. PATENT NO. DATE KIND US 3229471 PRIORITY APPLN. INFO.: 19611218 19660118 US 1961-160066 US

L8 ANSWER 2 OF 8 CAPLUS COPYRIGHT 2007 ACS on STN .

AB Ethylene (I) and propylene (II) are separated from the raw gas, formed from pyrolysis of hydrocarbons, by washing the raw gas at 8-12 atmospheric with a N-alkyl-y- or 8-lactam to dissolve acetylenes, diolefins, H2S, S-containing organic compds. and C4 hydrocarbons. The

washed gas contains I, II, H2S, CO, H, CH4, CO2, ethane, propane, and butane. Preferred lactam for washing is N-methylpyrrolidinone (III).

washed gas is treated with an aqueous alkali solution to remove traces

is and CC2. The purified gas is compressed to 25-35 atmospheric, and either condensed by cooling it at very low temperature, or absorbed by a

liquid. The condensate or the solution is distilled to give pure I and II. The

absorbed by III, namely, acetylene, diolefins, H2S, S-containing organic compds

and a part of CO2, are regenerated by evaporation. The regenerating column is

an is a continuous distillation column, fed with the washing liquor and with steam at such a rate that at the head of the column a part of water and the regenerated components are distilled. The III in the residue contains 1-10% water. The hot residual III is dehydrated by bubbling through it a part of CN4 and of N, released in the purification. Acetylene and diolefins are partly polymerized during the regeneration. The immortion

dioletins are percey, processing of the plant is given.

ACCESSION NUMBER: 1966:419864 CAPLUS

DOCUMENT NUMBER: 65:19864,

ORIGINAL REFERENCE NO.: 65:3649f-h Separation of ethylene and propylene from raw pyrolyzed gas Thormann, Kurt Metallgesellschaft A.-G. TITLE:

INVENTOR (S): PATENT ASSIGNEE (S):

SOURCE: 5 pp. DOCUMENT TYPE: Unavailable

LANGUAGE: FAMILY ACC. NUM. COUNT: PATENT INFORMATION:

PATENT NO. KIND DATE APPLICATION NO. DATE 19641223 19600623 DE 1183902 PRIORITY APPLN.. INFO.: DE 1960-M45718 19600623

ANSWER 4 OF 8 CAPLUS COPYRIGHT 2007 ACS on STN
Oxidation products, e.g. ethylene oxide, acrolein, and methacrolein, are
prepared by the controlled catalytic oxidation of corresponding olefnic
hydrocarbons with O. For example, the reaction mixture obtained by the
catalytic oxidation of propylene with O in the vapor phase in the
presence of a Cu2O catalyst and quenching with M2O contains essentially
2.6% acrolein, 34.2% propylene and propane, 0.6% O,
19.4% permanent gases, and 43% water. The mixture is cooled from
149° to 49° in 2 stages. Two separate liquid condensates
are obtained, the first containing 8.6% acrolein and 76% water and the
nd

containing 4.2% acrolain and 13% water. The remaining vapor phase

contains
87% acrolein, 1.3% water, the hydrocarbons that are gaseous under normal
conditions, and the permanent gases of the reaction mixture The vapor

is compressed from its pressure of 5.6 atmospheric to 21 atmospheric and

introduced into an absorption tower at the bottom. A jet of water is introduced at the top. The first liquid condensate, separated during the quenching of the reaction mixture, is introduced into the absorption

at a place midway between the water inlet and the vapor phase inlet. The absorption tower is maintained at 21 and 21 atmospheric Acrolein is selectively absorbed by the aqueous solvent, forming a solution of water

acrolein in a proportion of 50.1 moles/water/mole acrolein. The games leaving at the top of the tower contain essentially propylene, propane, and permanent gases. The absorption solution is withdrawn from the bottom of the tower and is distilled with the second condensate. The top fraction from the distillation contains acrolein and a relatively small amount of water. More than 99% acrolein is recovered

the reaction mixture. The aqueous phase at the bottom of the column is partially

returned to the absorption tower. A total of 17.6 moles water are introduced at the top of the tower per mole of acrolein which is

recovered

by distribution If this reaction is conducted under essentially the
same conditions, with the exception that the vapor phase is introduced
into the absorption tower without previous compression and both liquid
condensates are distribled directly in the distribution column, 35.2 mol
water are required per mole acrolein to obtain an equivalent yield of

1964:16023 CAPLUS
60:16023 .
60:2772a-e
Recovery of water-soluble oxidation products of hydrocarbons
Courter, Martin L.: Thayer, David S.
Shell Internationale Research Maatschappij N. V.
6 pp. INVENTOR(S):
PATENT ASSIGNEE(S):
SOURCE:
DOCUMENT TYPE:

6 pp.
Patent
Unavailable LANGUAGE FAMILY ACC. NUM. COUNT: PATENT INFORMATION:

> DATE PATENT NO KIND APPLICATION NO. 19630502 19610406 DE 1147932 US 3097215 DE 1961-573353 US 1960-21003

ANSWER 6 OF 8 CAPLUS COPYRIGHT 2007 ACS ON STN
A normally gaseous hydrocarbon component is separated from a mixture of ally

ally gaseous hydrocarbons by introducing the mixture into a distillation zone. A bottom fraction and a vaporous overhead fraction are withdrawn from the distillation zone. A portion of the overhead fraction, which comprises the component which is to be separated, is compressed and thereby heated. A portion of the compressed overhead fraction, which has been further heated or cooled, is brought into contact indirectly with liquid from the lower portion of the distillation zone thereby heating and partially vaporizing the liquid from the distillation zone thereby heating and partially vaporizing the liquid from the distillation zone thereby heating and catillation zone, while the vaporized liquid may be used to reboil the distillation zone. This process may be used in the separation of C2H4 from C2H6 in a C2-splitting operation or for

The seperation of C3H6 from C3H8.

ACCESSION NUMBER: 1962:455562 CAPLUS DOCUMENT NUMBER: 57:55562

ORIGINAL REFERENCE NO: 57:10979acc

TITLE: Gas appared

57:10979a-c
Gas separation, especially in production of ethylene
and propylene
Greco, Javerio G.
M. W. Kellogg Co.
6 pp.
Patent

INVENTOR(S): PATENT ASSIGNEE(S):

SOURCE: DOCUMENT TYPE: LANGUAGE: Unavailable

FAMILY ACC. NUM. COUNT: PATENT INFORMATION:

PATENT NO. KIND DATE APPLICATION NO. DATE 19561115 19561115 US 3000188 PRIORITY APPLN. INFO.: 19610919 US 1956-622291

ANSWER 5 OF 8 CAPLUS COPYRIGHT 2007 ACS on STN
Chilling of alkylation mixts, rich in isobutane is accomplished by flash
vaporization or "self refrigeration." Vapors rich in isobutane are then
compressed and fed to high-pressure fractionating towers and
isobutanerich liquids returned to the reactors. The temperature of the under the proposed conditions is maintained lower than usual and under the proposed conditions is mainteaned acress successful or of acidic components in the alkylate is reduced during despobutanization. Of acidic components in the alkylate is reduced during despobutanization. The inobutane and colefinic material are treated with a catalyst in the liquid phase at <100°F. With a H2SO4 catalyst, alkylation temps, of 30-55°F, are preferred. The alkylatable material is usually an olefinic hydrocarbon, e.g. propylene or butylene, or it may be an alkyl ester. For example, 30.2 bbl. propylene, 19.2 bbl. butylene, and 539.8 bbl. isobutane were treated in the liquid phase at 50 lb./in.2 gage with 92% H2SO4. The reaction mixture was cooled by indirect. indirect
heat-exchange with flashed effluent hydrocarbons, separated, and
deisobutanized.
ACCESSION NUMBER: 1963:440793 CAPLUS 1963:440793 CAPLUS
59:40793
59:7292f-g
Alkylation of olefinic hydrocarbons
Davies, James A.
Texaco Inc.
4 pp.
Patent DOCUMENT NUMBER: ORIGINAL REFERENCE NO.: TITLE: INVENTOR(S): PATENT ASSIGNEE(S): SOURCE: DOCUMENT TYPE: LANGUAGE: Unevailable FAMILY ACC. NUM. COUNT: PATENT INFORMATION: PATENT NO. KIND DATE APPLICATION NO. DATE US 3097250 PRIORITY APPLN. INFO.: 19630709 US 1960-39370 US 19600628

ANSWER 7 OF 8 CAPLUS COPYRIGHT 2007 ACS on STN
Isobutane (50-90 volume % of the hydrocarbon charge) and olefins, such as propene, react in the liquid phase in the presence of a nonvolatile alkylation catalyst, e.g. H2504 (88-94 weight % tirratable acidity). The temperature and pressure conditions (30-75'F. and 0-30 lb./sq. in. gage are such that part of the isobutane and practically all of the C3H8 and lighter products are evaporated to give effective refrigeration for the alkylation zone. The alkylator delivers a depropanized liquid emulsion to be settled and caustic-washed free of acid. This alkylate passes to the top of a distillation tower where butanes are distilled from the downcoming alkylate and returned to the alkylator. The isobutane-rich vapors from the alkylator containing C3H8

compressed (40-130 lb./sq. in. gage) and condensed with cooling water. The condensate is depropanized, and the isobutane-rich bottoms

returned to the alkylator.
ACCESSION NUMBER: 1962:443938 CAPLUS
DOCUMENT NUMBER: 57:43938
ORIGINAL REFERENCE NO.: 57:8811f-h

Catalytic alkylation of olefins with isobutane
Texaco Development Corp. PATENT ASSIGNEE (S):

9 pp. Patent DOCUMENT TYPE:

LANGUAGE: Unavailable

PATENT INFORMATION:

PATENT NO. KIND DATE APPLICATION NO. DATE GB 895178 PRIORITY APPLN. INFO.: 19600505 19590511 19620502 GB 1960-15908

ANSWER 8 OF 8 CAPLUS COPYRIGHT 2007 ACS on STN
The liquid mixture of hydrocarbons containing olefins, e. g.,
propane and propylene, is freed of these components by
successive decantations in a specially designed apparatus. There the
thic propane and propylene, is freed of these components by successive decantations in a specially designed apparatus. There the olefinic components and the esterifying solution (a 75% H2504 solution) are allowed to circulate in countercurrent manner by means of flowing in an inert gas preliminarily compressed. The temperature in the battery is 40° and the pressure 20 kg. per sq. cm. At one end of the battery is collected a liquid containing saturated hydrocarbons and practically free of olefins, and at the other an esterifying solution saturated with olefin slc. which is caused to appear there by dilution and heating. The liberated alcs. are isolated by suitable means, e. g., distinguished alcs. are isolated by suitable means, e. g., distinguished alcs. Saturated alcs. are isolated by suitable means, e. g., distinguished alcs. are isolated by suitable means, e. g., distinguished alcs. are isolated by suitable means, e. g., distinguished alcs. are isolated by suitable means, e. g., distinguished alcs. are isolated by suitable means, e. g., distinguished alcs. are isolated by suitable means, e. g., distinguished alcs. are isolated by suitable means, e. g., distinguished alcs. are isolated by suitable means, e. g., distinguished alcs. are isolated by suitable means, e. g., distinguished alcs. are isolated by suitable means, e. g., distinguished alcs. are isolated by suitable means, e. g., distinguished alcs. are isolated by suitable alcs. a

KIND DATE APPLICATION NO. PATENT NO. US 2345114

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